

# Decarbonising trucks, trains, boats and planes

## REA's Renewable Transport Fuels Group

Other RFNBO gases, are they a good idea,  
can their costs come down and which are most promising?

**Dr Keith Simons**

December 2019



# SHV Holdings trading group

*Privately owned, international in reach and local in focus*



SHV Energy is part of SHV Holdings, a family owned Dutch trading company, regarded as one of the world's largest private trading groups.

SHV Holdings is a highly diversified company

**makro**

**ERIKS**

 **MAMMOET**

 **nutreco**



 **NPM CAPITAL**

 **SHV ENERGY**

SHV Holdings employs around 60,000 people in 60 countries.

Est.  
1896

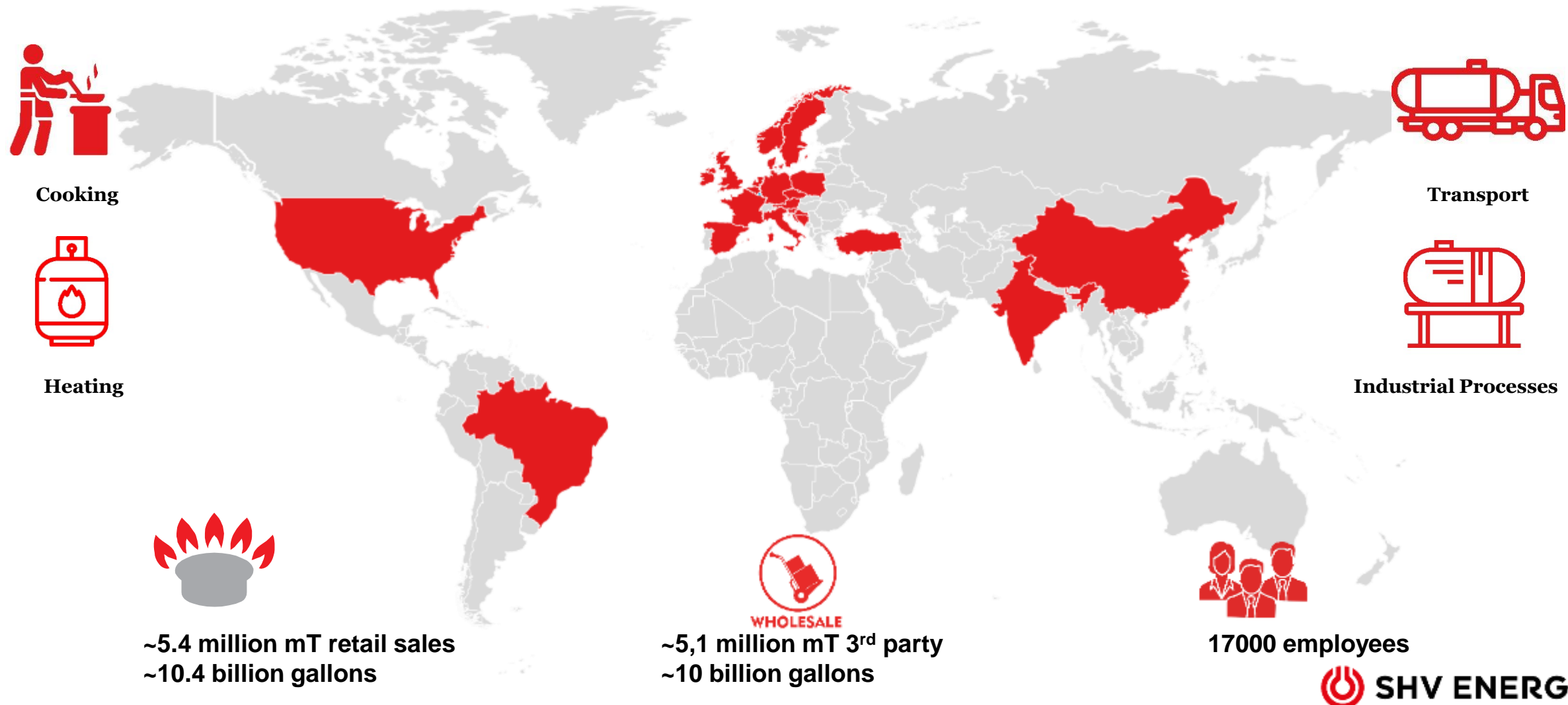
60  
Countries

60,000  
Employees

€20B  
Turnover  
2017

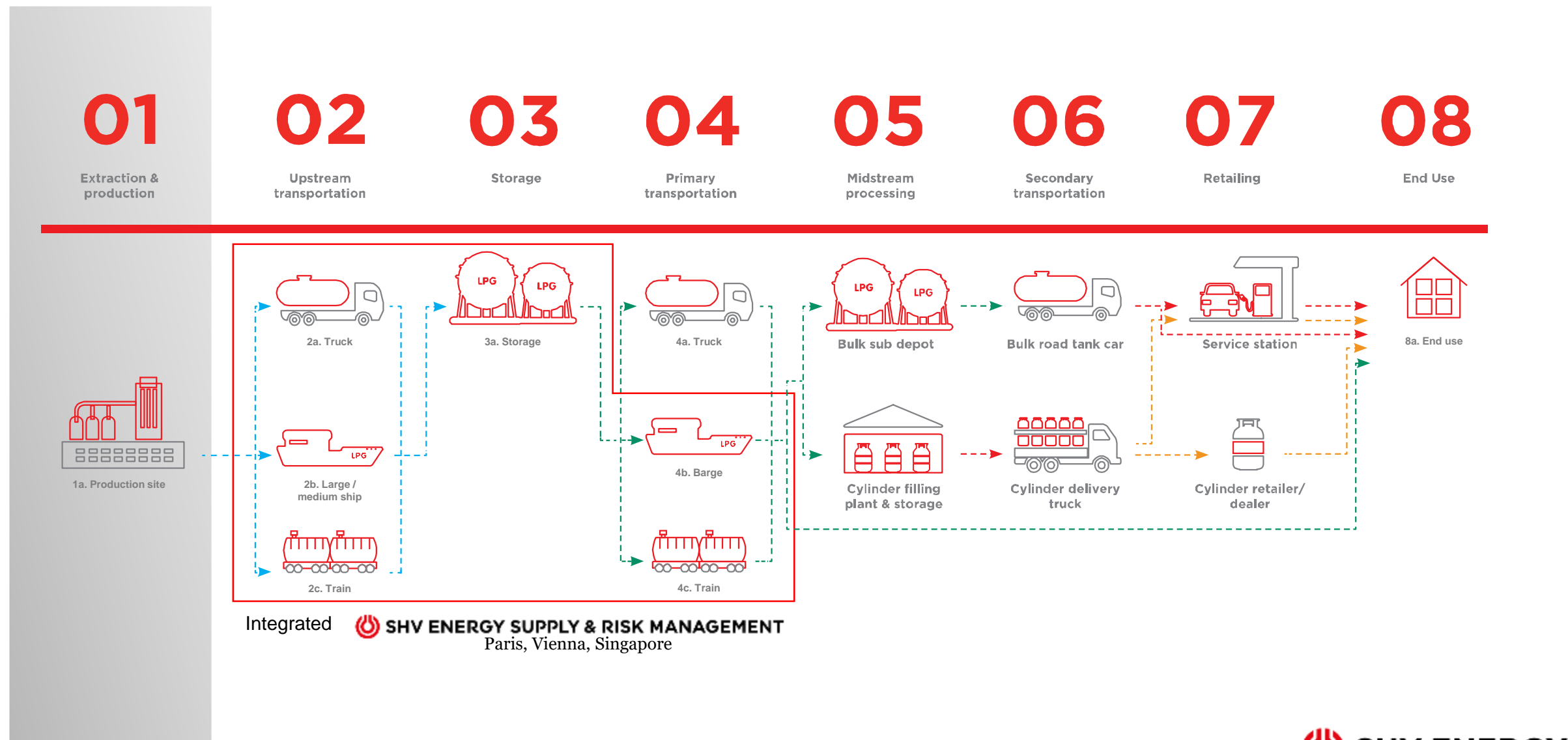
 **SHV ENERGY**

# SHV Energy : Our global brands



Source: SHV Energy 2017 report

# Our value chain / logistics



# Our product portfolio innovation

*The past*

**Coal**



1896

**LPG  
Propane  
Butane**



1950

**Biomass**



2008

*The present ...*

**LNG**



2013

*& the future ...*

**BioLPG  
Renewable  
Propane**



2018



2019

**Our Vision : Advancing Energy Together**

**Our commitment : 5 million tonnes of CO2 reduction by 2025**

**Our bold ambition : 100% of our energy products to be from renewable sources in 2040**



# UK Rigid Truck Types



2 axle <18te



18-26te 3 axle



8 x 4 tipper 28-32te



2 axle 16te Flatbed



3 axle Concrete mixer



Curtainsider

# The World's 1st LPG Range-Extended Electric 16te Cylinder truck

Military grade Li-Ion batteries

2 litre **LPG** steady state engine (could also run on CNG)

Plug-in charging (1.5 h @ 44kW)

40 mile EV-only range with GPS ring-fencing

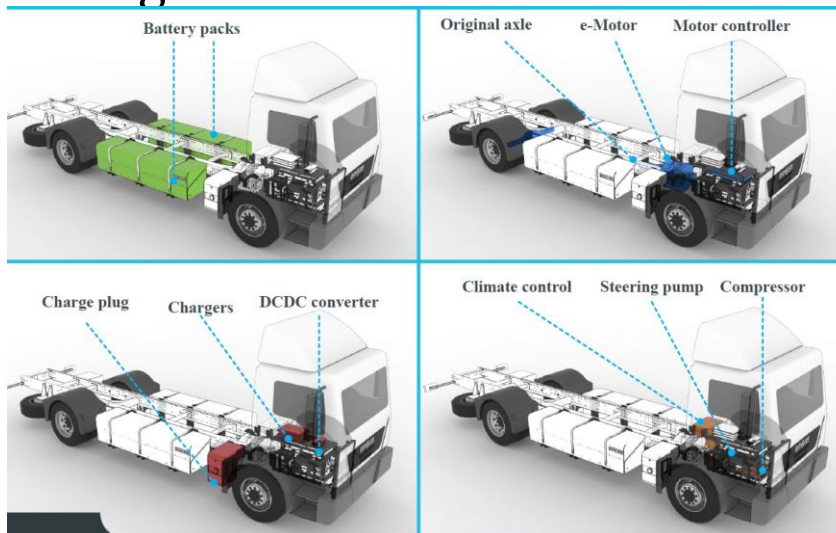
350 mile RE range

Regenerative braking

Cleaner

Quieter (50%)

Lower carbon



# Other RFNBO gases.....

(Renewable Fuels of Non  
Biological Origin)

## Definition of RFNBOs

- 3.33 RFNBOs are renewable liquid or gaseous transport fuels for which none of the energy content of the fuel comes from biological sources. These fuels are considered renewable where the energy content of the fuel comes from renewable energy sources but excluding bioenergy sources<sup>23</sup>. This means that RFNBOs could be made using electricity and/or heat and/or cold from wind, solar, aerothermal, geothermal or water (including hydrothermal sources, waves and tides). RFNBOs cannot be derived from bioenergy sources and therefore would not be able to be derived from biomass, landfill gas, sewage treatment plant gas or biogases. As the available energy source of RFNBOs comes from the process energy, the input feedstocks must contain no usable energy. In practice this means that the feedstock must be either water and/or carbon dioxide (CO<sub>2</sub>).
- 3.34 The simplest RFNBO is renewable hydrogen (for example from wind or solar power electrolysis) that is directly used in transport applications: either in an internal combustion engine or a fuel cell electric vehicle. A range of other renewable transport fuels can also be generated by reacting this RFNBO hydrogen precursor with CO<sub>2</sub>, to produce RFNBO products such as methane, methanol, ethanol, di-methyl ether, petrol, kerosene and diesel.
- 3.35 If a RFNBO is produced from CO<sub>2</sub>, the carbon dioxide can come from waste fossil sources (for example, waste flue gases from coal and natural gas power generation or similar industrial combustion processes), from biological sources (e.g. alcohol fermentation or anaerobic digestion) or from atmospheric or naturally-occurring/geothermal sources.

## RTFO Guidance Part One Process Guidance 2019: 01/01/19 to 31/12/19

Moving Britain Ahead

This definition would also allow for ammonia (NH<sub>3</sub>)

# Other RFNBO Gases (Renewable Fuels of Non Biological Origin)

Methane

Dimethyl Ether (via Methanol)

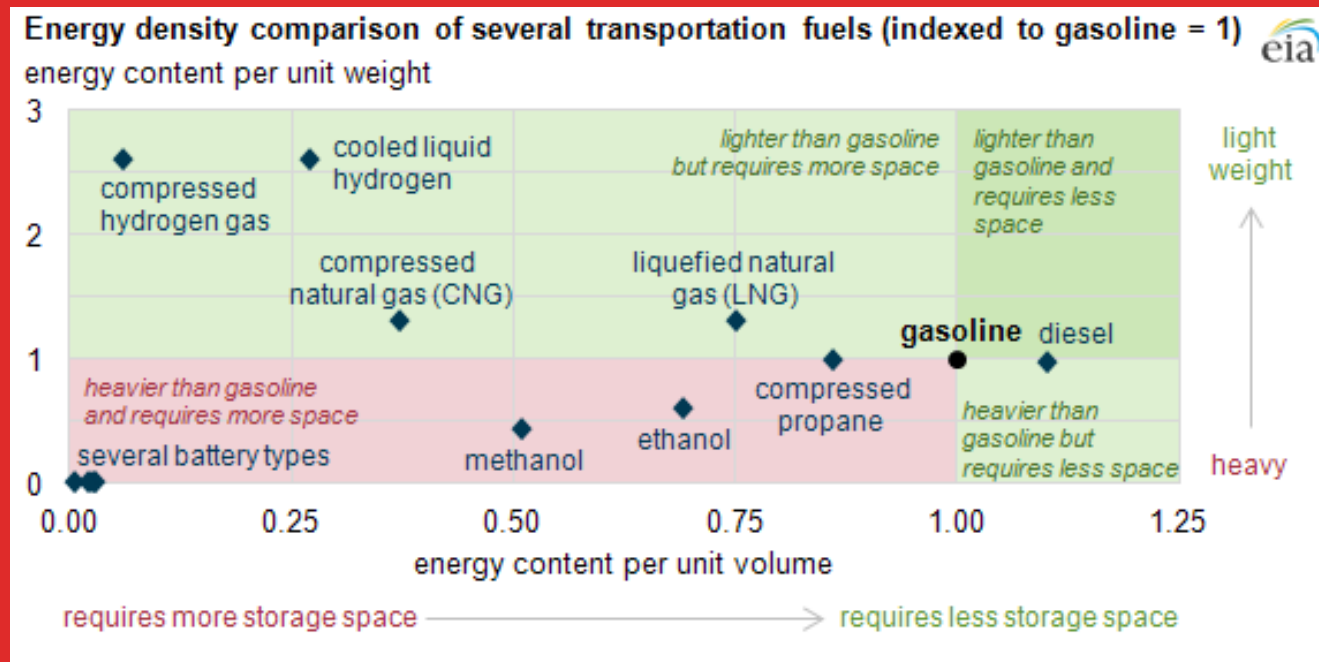
LPG?

(NH<sub>3</sub>)



# Are they a good idea?

## If you don't have a direct need for the energy



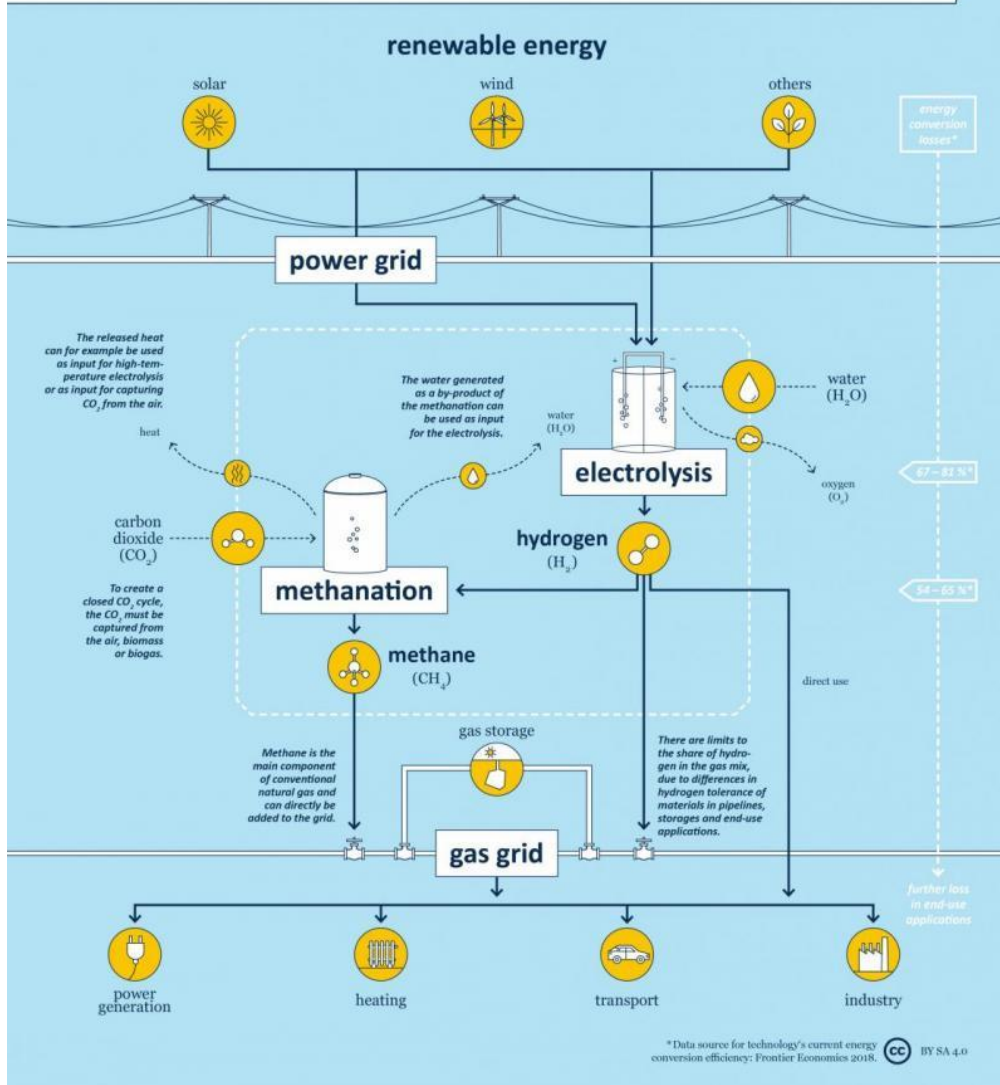
## If you don't need to store and then transport – Yes!

# Methanation

## Power-to-gas

[PtG, P2G] Producing electricity-based synthetic gas for a renewable energy system

CLEAN  
ENERGY  
WIRE



Makes a drop-in fuel

Can benefit from surplus electricity

Can store energy over a long period of time

Transports well

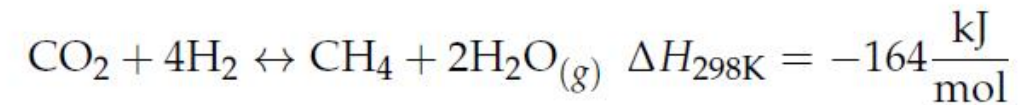
Doesn't require biomass

Can re-use a lot of (downstream) existing infrastructure

Many demonstration projects

However

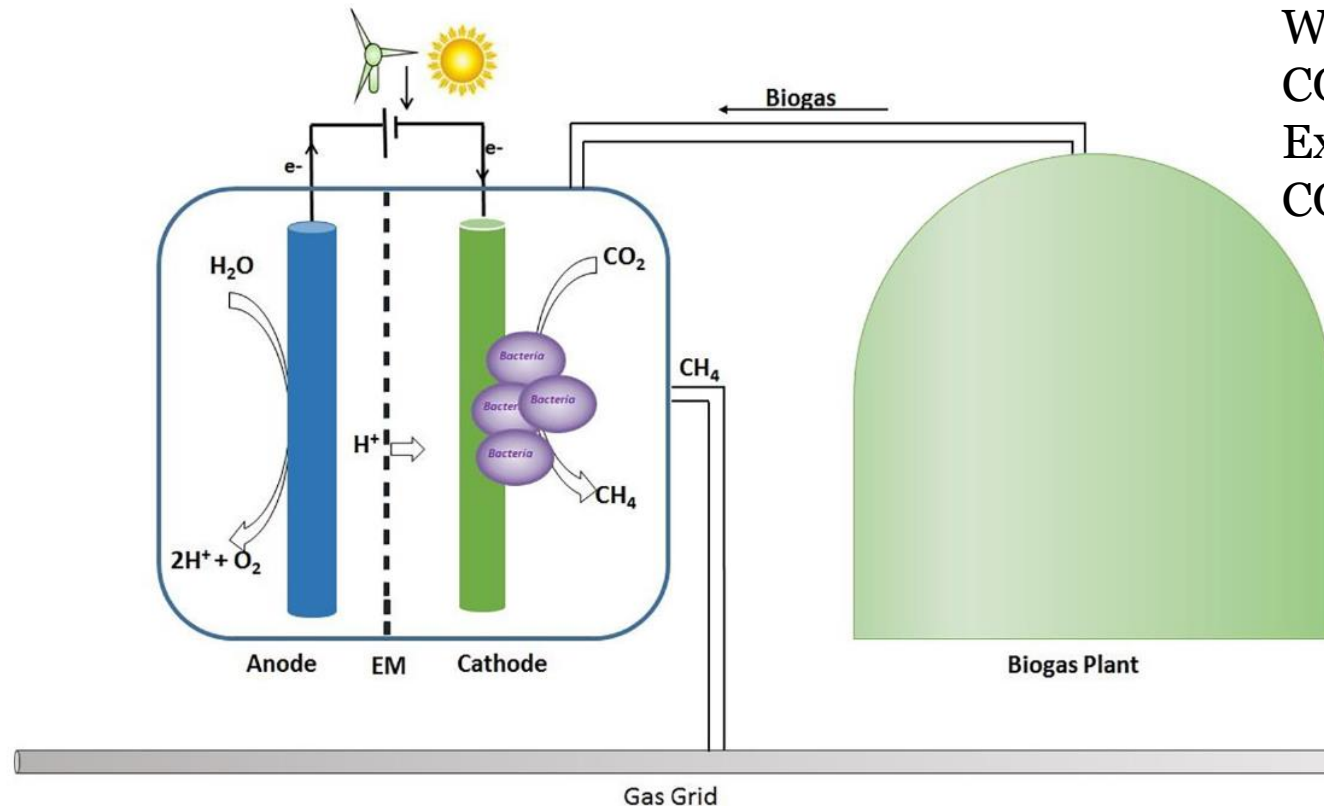
- after electrolysis only about 67-81% of energy remains
- After methanation only about 54-65% of energy remains
- Makes expensive water (from water)
- Requires a point source of ( clean) CO<sub>2</sub>
- Not suited to intermittent production



# Power to Gas - Bioelectrochemical biogas upgrading

N. Aryal et al.

Bioresource Technology xxx (xxxx) xxx-xxx



Will the release of biogenic CO<sub>2</sub> from biogas be allowed in the future? Exploit (constrained) electricity to methanate CO<sub>2</sub> in biogas in microbial fuel cells

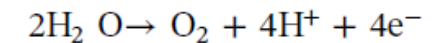
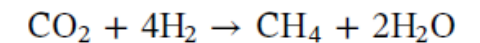
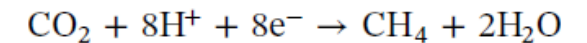


Fig. 3. Bioelectrochemical CH<sub>4</sub> enrichment phenomena discussed in this review, where EM represent Exchange membrane, electrochemical oxidation reaction takes place at the anode to generates O<sub>2</sub> and H<sup>+</sup> and electrochemically active microorganisms utilize the cathode as electron donor and CO<sub>2</sub> from biogas to produce CH<sub>4</sub>.

# Biogas enrichment in anaerobic digestion

N. Aryal et al.

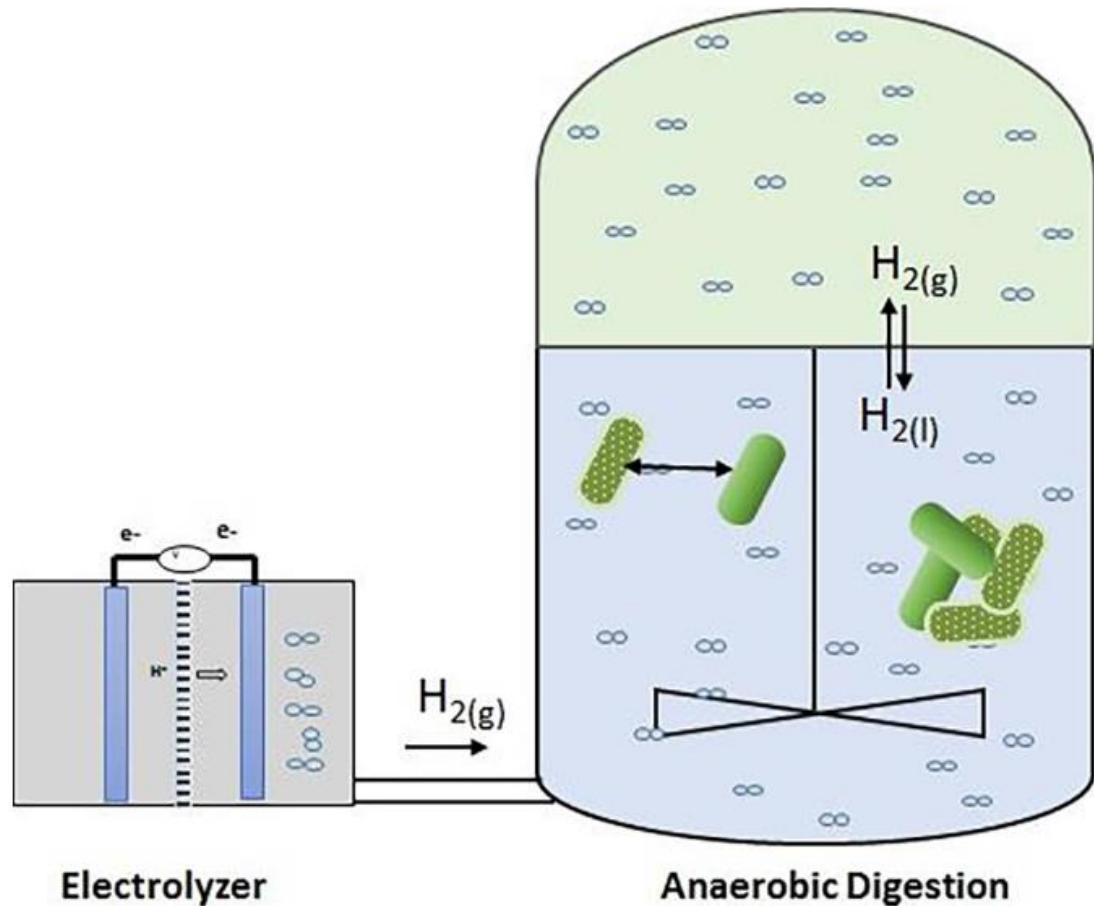


Fig. 2. Hydrogen ( $H_2$ ) uptake in AD supplied from electrolyzer where “ $\circ\circ$ ” is  $H_{2(g)}$  represents in gaseous phase, and  $H_{2(l)}$  in the liquid phase.

Hydrogen from a conventional electrolyser injected into digester and methaneates  $CO_2$  in biogas

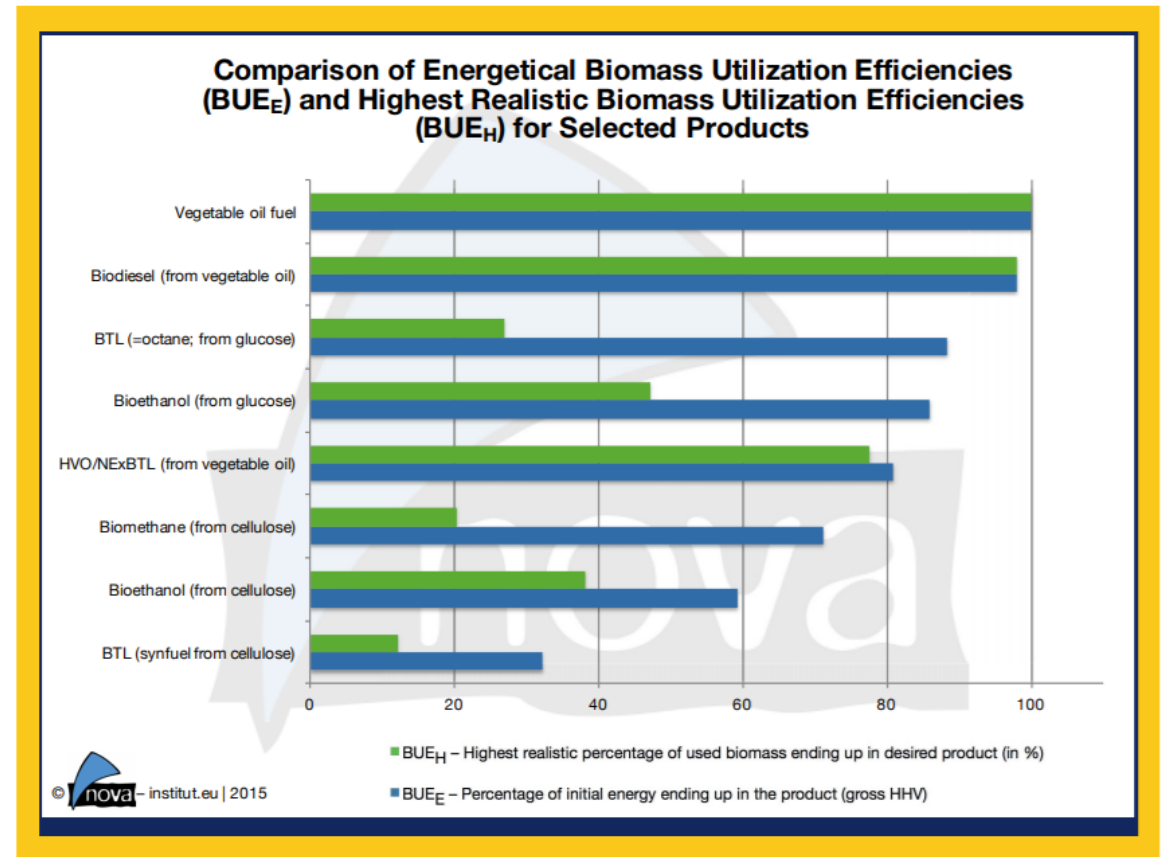


Figure 4: Comparison of Energetic  $BUE_E$  with Highest Realistic  $BUE_H$  for selected compounds

# Dimethyl Ether (from Methanol)

Companies such as CRI in Iceland have been pioneering Methanol synthesis from electrolytic hydrogen and CO<sub>2</sub> flue gas

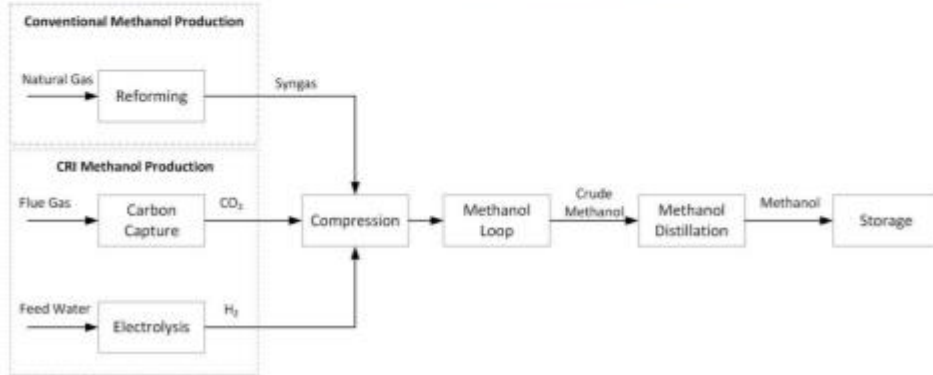
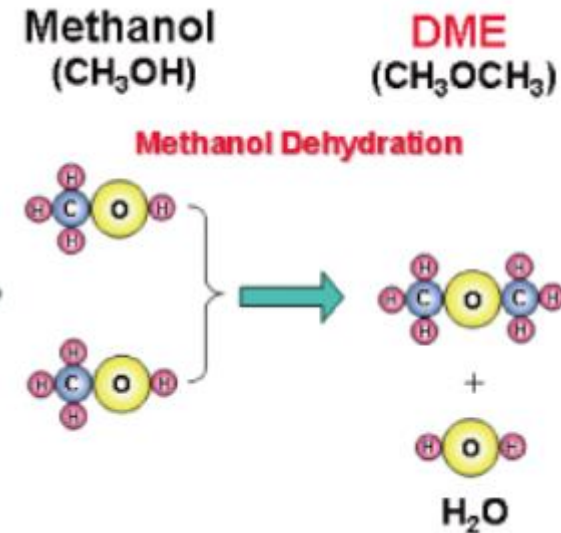


FIGURE 1 | (Top) CRI's George Olah Renewable Methanol plant in Svartsengi, Iceland. (Bottom) Block flow diagram showing the different origins of syngas for the conventional process compared to the CRI process starting from CO<sub>2</sub> pointing out the energy intensive reforming process in the former.



## Process Advantages of Direct CO<sub>2</sub> to Methanol Synthesis

Dana S. Marlin\*, Emeric Sarron and Ómar Sigurbjörnsson

Carbon Recycling International, Kópavogur, Iceland

# DME has very similar properties to LPG

- DME is promising as Energy carrier from remote resource for high energy intensity by volume and safety aspect.

	Liquid H <sub>2</sub>	Liquid Ammonia	Methanol	DME	CO <sub>2</sub>
Formula	H <sub>2</sub>	NH <sub>3</sub>	CH <sub>3</sub> OH	CH <sub>3</sub> OCH <sub>3</sub>	CO <sub>2</sub>
Liquid density [kg/L]	0.07	0.7	0.795	0.67	1.1
Boiling point [°C] @0.1Mpa	−253	−33.4	64.4	−25	(−50)*1
Vapor pressure [Mpa] @25°C	—	1.02	0.0129	0.53	(0.7)*1
Energy density by Weight [MJ/kg]	120.8	19.2	21.1	28.8	—
Energy density by Volume [MJ/L]	8.5	13.4	16.8	19.3	—
Explosion limit [%]	4~75	15~28	6.7~36	3.4~27	—
Allowable limit of toxicity	—	25ppm	200ppm	—	—

\*1: Marine transportation condition of liquid CO<sub>2</sub>



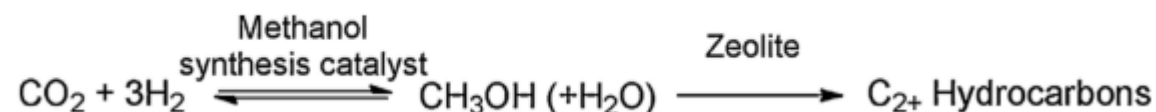
Japan DME Forum



# LPG Synthesis?

Synthesis of C<sub>2+</sub> hydrocarbons by CO<sub>2</sub> hydrogenation over the composite catalyst of Cu–Zn–Al oxide and HB zeolite using two-stage reactor system under low pressure

Masahiro Fuiiwaru<sup>\*</sup>, Hiroaki Sakurai, Kumi Shiokawa, Yasuo Iizuka



**Table 2**

CO<sub>2</sub> hydrogenation over Cu–Zn–Al (6:3:1) oxide + HB composite catalysts using two-stage reactor system.<sup>a</sup>

Run	Temp. of first reactor (°C)	Pressure (MPa)	Flow rate (mL/min)	CO <sub>2</sub> conv. (%)	Selectivity (C-mol%)								C <sub>2+</sub> yield (C-mol%)	
					CO	C <sub>1</sub>	C <sub>2</sub>	C <sub>3</sub>	C <sub>4</sub>	C <sub>5+</sub>	MeOH	DME		
1	250	0.98	50	25.3	91.3	0.2	1.4	1.5	1.5	0.3	2.4	1.4	1.19	
2 <sup>b</sup>	250	0.98	50	20.7	73.2	1.3	1.2	5.9	12.0	1.7	3.1	1.6	4.31	
3	300	0.98	50	32.5	90.8	0.3	1.4	2.7	2.7	0.5	1.1	0.5	2.37	
4	400	0.98	50	43.2	87.6	0.5	1.4	5.0	4.5	0.5	0.4	<0.1	4.92	
5	420	0.98	50	45.9	85.4	0.8	1.3	5.9	5.6	0.6	0.3	<0.1	6.15	
6 <sup>c</sup>	420	0.98	50	45.8	87.1	0.7	1.3	5.2	4.9	0.5	0.2	<0.1	5.45	
7 <sup>d</sup>	420	0.98	50	45.8	89.3	0.4	0.6	0.7	1.2	0.3	2.4	5.1	1.28	
8 <sup>e</sup>	420	0.98	50	45.2	95.2	0.4	0.7	1.6	1.8	0.2	0.1	<0.1	1.94	
9 <sup>b</sup>	420	0.98	50	25.0	95.7	0.7	1.0	0.2	0.0	0.0	1.8	0.6	0.30	
10 <sup>f</sup>	420	0.98	50	47.2	77.5	0.9	1.1	9.0	10.2	1.0	0.2	0.1	10.05	
11 <sup>f</sup>	420	0.98	25	47.8	66.8	1.4	1.7	15.0	13.6	1.3	0.2	<0.1	15.10	
12 <sup>f</sup>	420	0.5	50	45.2	93.5	0.3	0.5	2.6	2.5	0.4	0.1	0.1	2.71	
13 <sup>f</sup>	420	0.3	50	43.2	95.3	0.2	0.4	1.8	1.8	0.3	0.1	0.1	1.86	

<sup>a</sup> Reaction conditions: catalyst in the first reactor 1 g of Cu–Zn–Al (6:3:1) oxide obtained by calcination at 500 °C for 4 h, catalyst in the second reactor 0.1 g of Cu–Zn–Al (6:3:1) oxide obtained by calcination at 500 °C for 4 h and 0.9 g of HB zeolite (SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> = 28.5), 300 °C, 0.98 MPa, H<sub>2</sub>/CO<sub>2</sub> = 3, catalytic activity after a time-on-stream of 1 h.

<sup>b</sup> Without the cold trap.

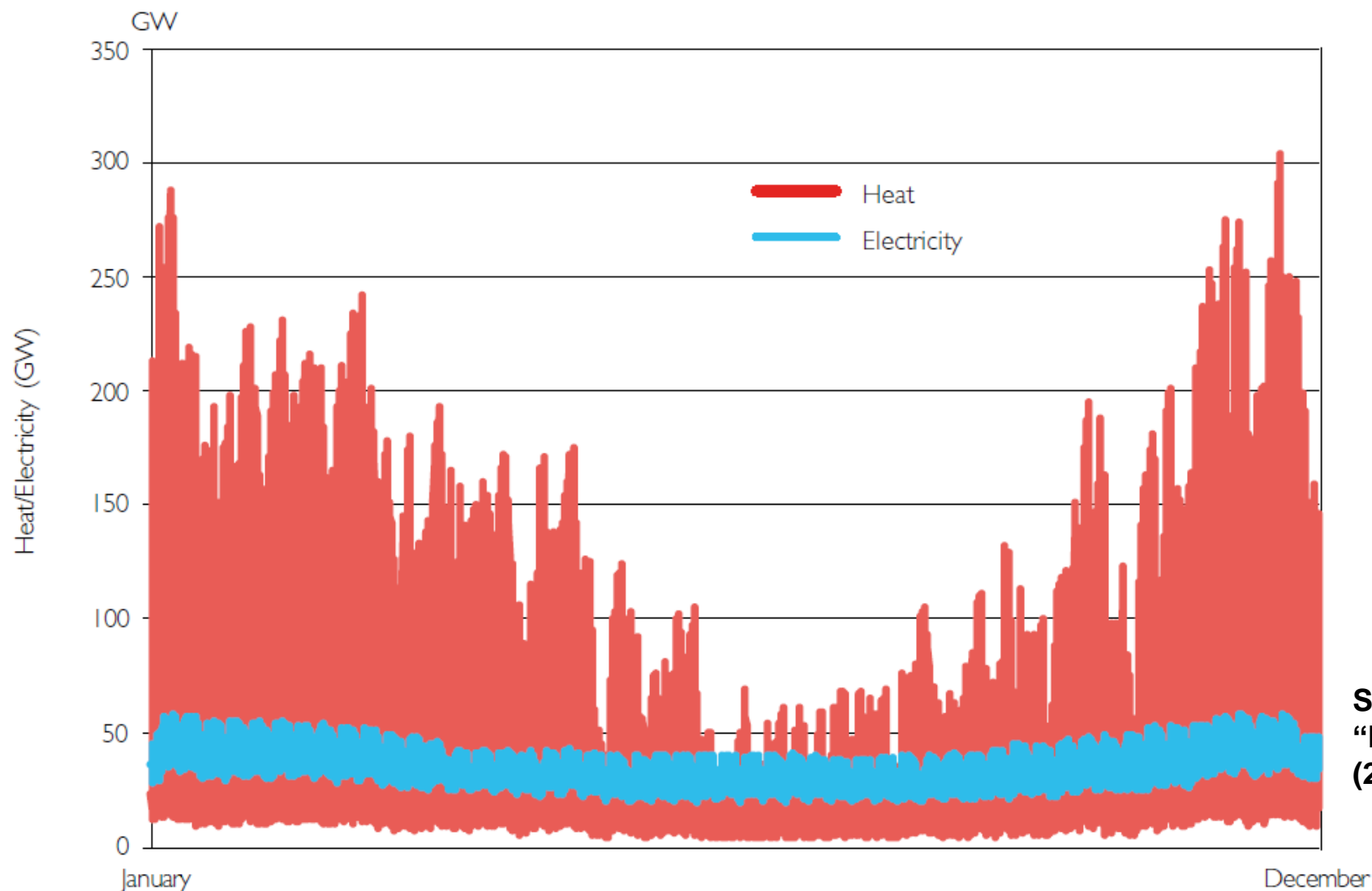
# Can their costs come down?

# (Competitive) efficiencies

P2G Pathways	Technologies	Current	Long Term
Power to Natural Gas End-users	Electrolyser, Low pressure hydrogen storage/ compression, Injection to pipeline to heat for residential to micro-CHP to large scale gas turbines	59–83%	64–86%
		52–76%	56–79%
		40–72%	55–74%
		18–26%	23–31%
Power to Renewable Content in Petroleum Fuel	Electrolyser, Low pressure hydrogen storage/ compression	55–83%	59–86%
Power to Power	Electrolyser, Low pressure hydrogen storage/ compression, fuel cell	17–40%	27–43%
Power to Seasonal Energy Storage to Electricity	Electrolyser, low-pressure compression, underground storage, Transmission pipelines, Natural gas-based power plants	16–24%	22–29%
Power to Hydrogen for zero—emission transportation	Electrolyser, low-pressure compression and storage, high-pressure compression for refueling station.	50–79%	54–82%
Power to Seasonal storage for Transportation	Electrolyser, low-pressure compression, underground storage, hydrogen separation technologies, high-pressure compression	36–68%	43–66%
Power to Renewable Natural Gas (RNG) to Pipeline (“Methanation”)	Electrolyser, Low-pressure energy storage and compression, Methanation reactor, Gas Clean-up, Injection of Renewable Natural Gas to the Natural Gas Pipeline	40–63%	45–65%
Power to Renewable Natural Gas (RNG) to Seasonal Storage	Electrolyser, low-pressure compression, Methanation reactor, Gas Clean-up, Underground storage, Injection of RNG to the Natural Gas Pipeline	34–60%	43–58%

Source: Transition of Future Energy System Infrastructure; through Power-to-Gas Pathways. *Energies*. (2017)

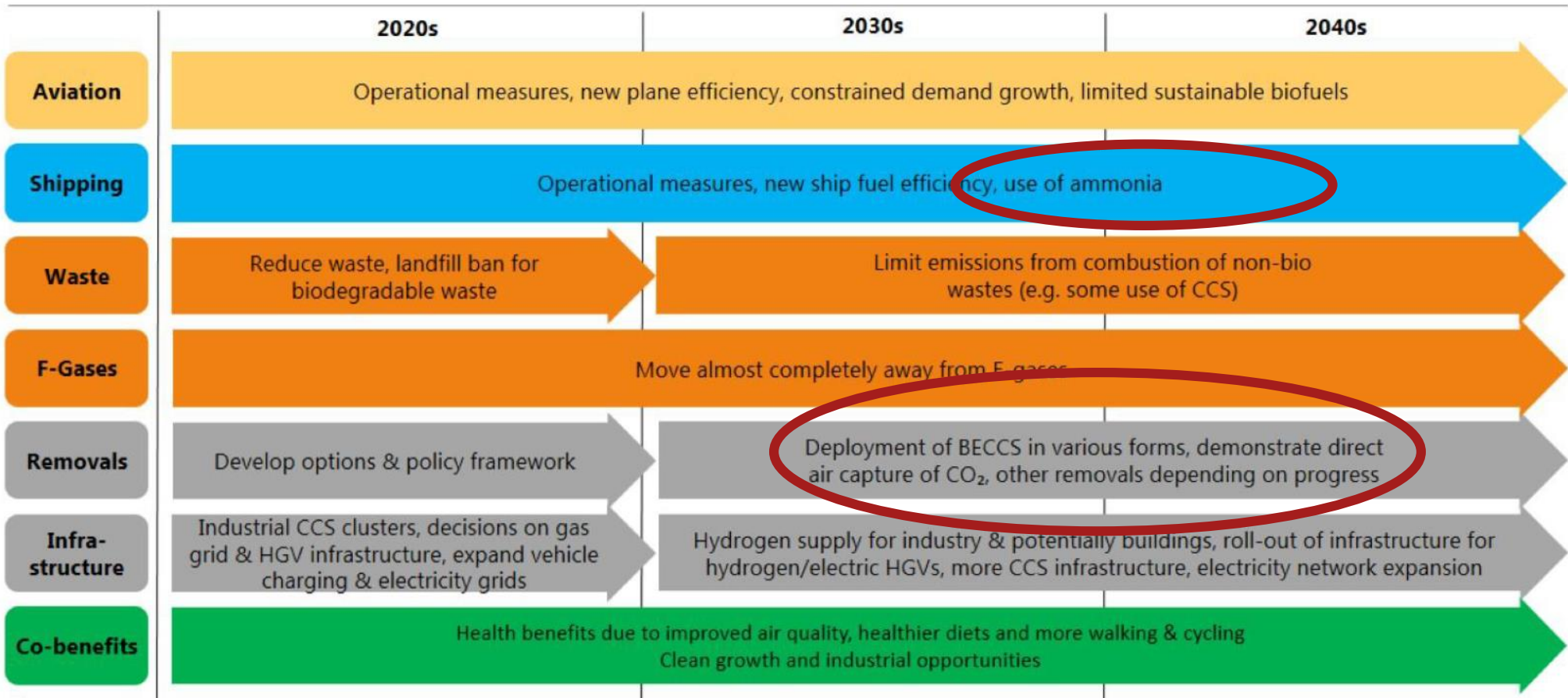
# Heat & electricity demand variability across the year



Source: DECC  
"Future of Heating"  
(2012)

# Reaching net-zero emissions in the UK

## How UK net-zero scenarios can be delivered



DAC: Having a strategy requires which relies on overcoming the Second Law of Thermodynamics is bad policy

# Exploitation of existing upstream and downstream infrastructure is a major cost saving

01

Extraction & production

02

Upstream transportation

03

Storage

04

Primary transportation

05

Midstream processing

06

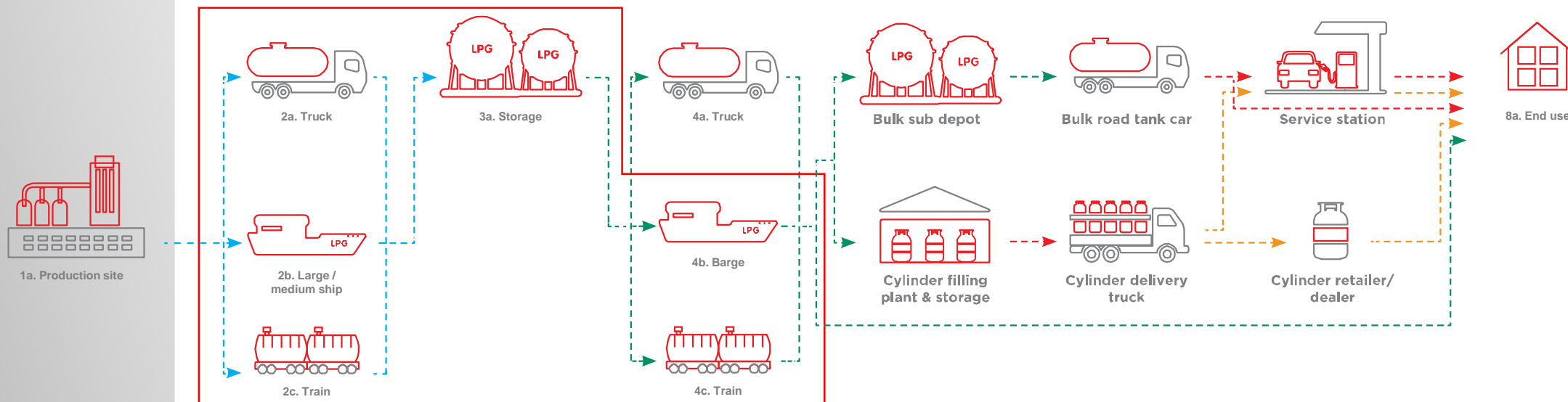
Secondary transportation


07

Retailing

08

End Use



Integrated  **SHV ENERGY SUPPLY & RISK MANAGEMENT**  
Paris, Vienna, Singapore

## Other developments

Massive expansion of (seasonal) renewable electricity and load/frequency response via hydrogen generation will drive down upstream costs

Expansion of CCS/CCU will again drive down costs

However, current policy is akin to “being more catholic than the Pope”

Require policy which encourages the fair exploitation of recycled carbon ***and carbon monoxide***



# RFNBO definition too narrow

CO<sub>2</sub> has no intrinsic energy content

CO<sub>2</sub> needs to be captured

Hydrogen/electrons used to make **carbon monoxide** – this is the actual fuel

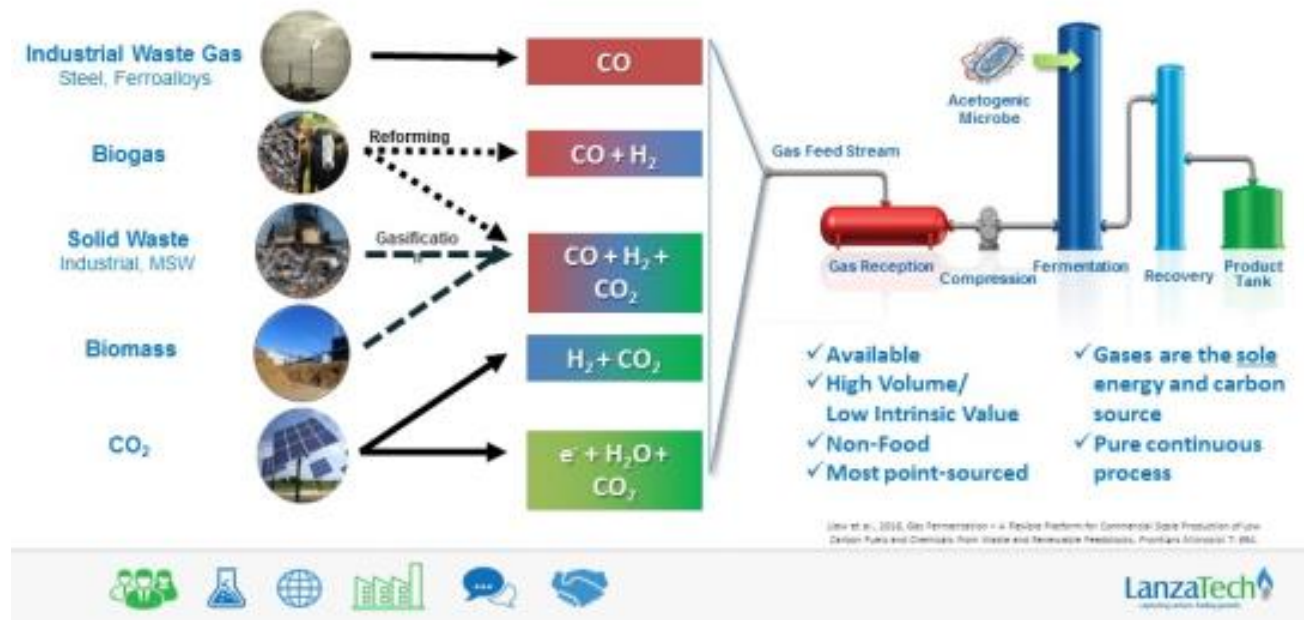
Maximisation of carbon monoxide is key

Further hydrogen then used to make fuels

Enables access to large point sources of carbon (and hydrogen) together with electrolytic hydrogen



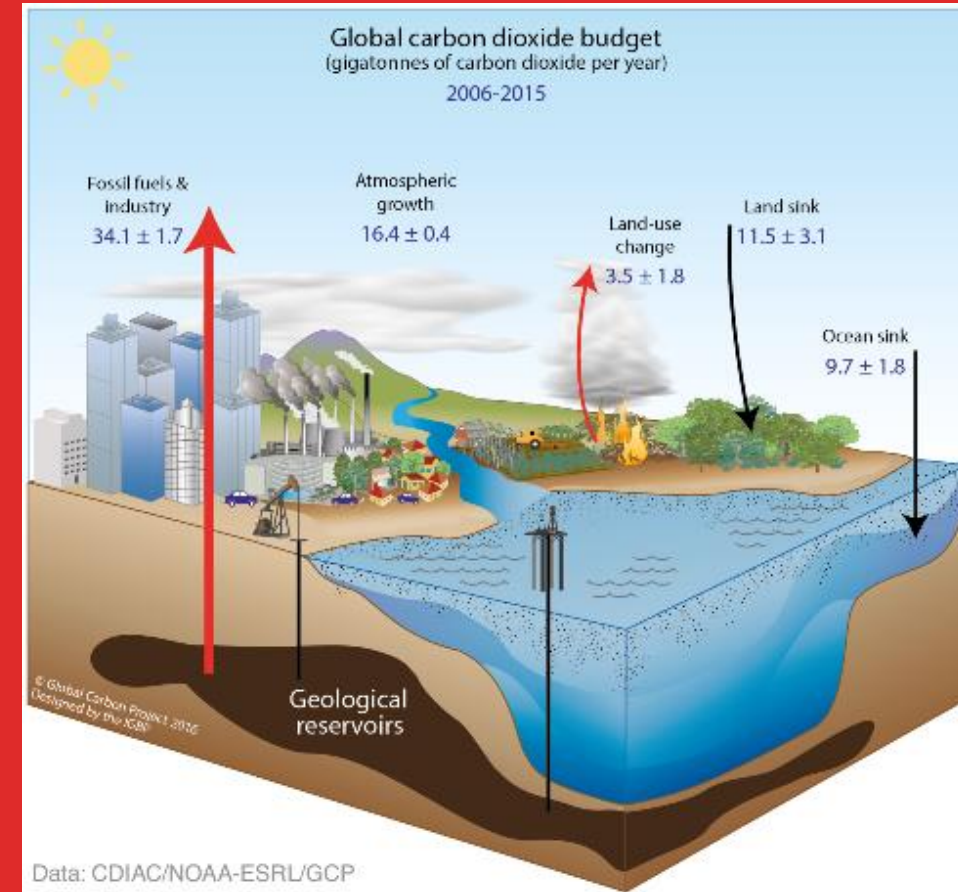
## Waste Carbon Streams as a Resource for Gas Fermentation



# Are they any good?

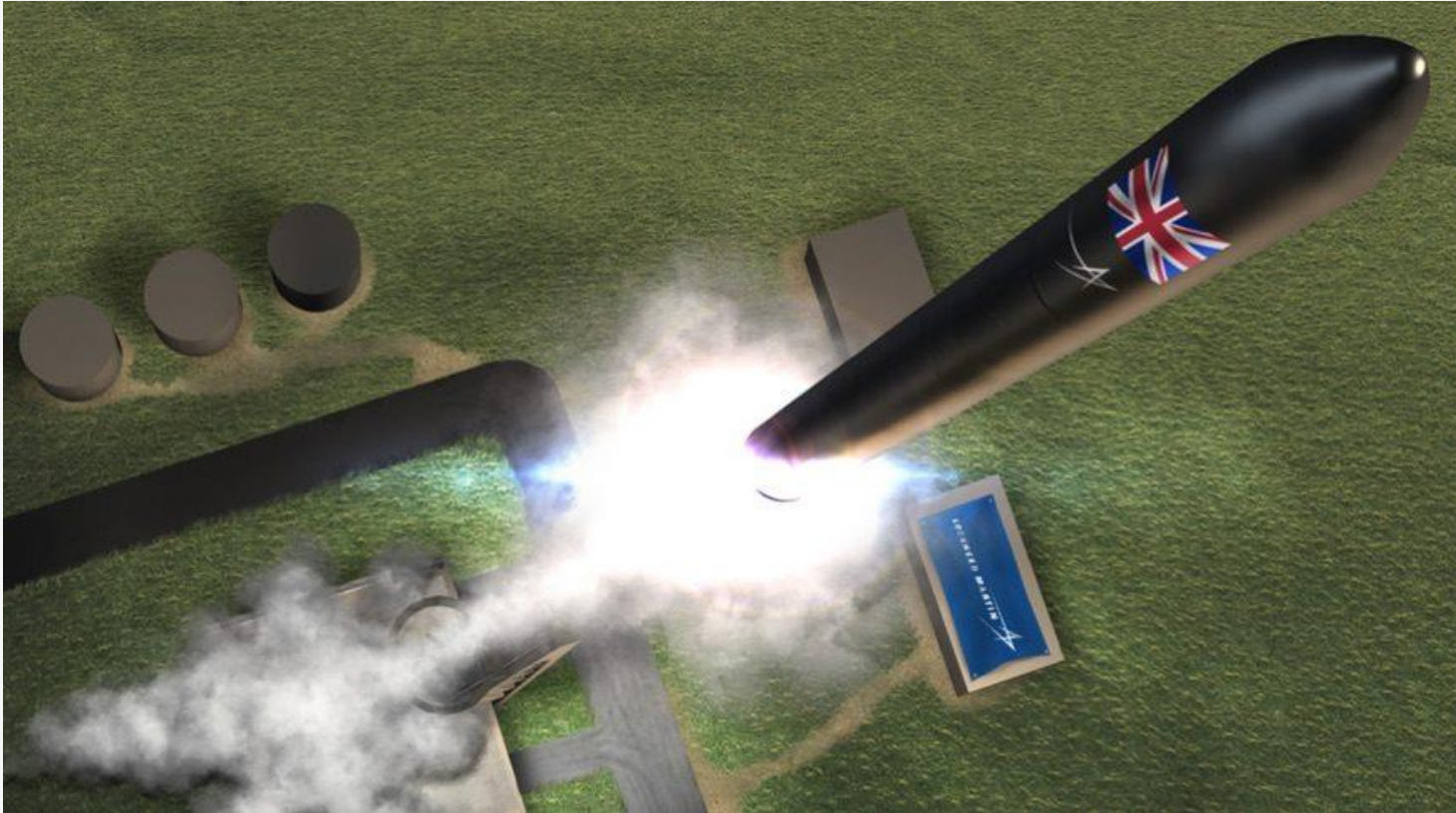
Climate science tells us that bread today is just as valuable as jam tomorrow

Quick wins with ***drop-in*** replacements have long-term cumulative benefit  
(can we please forget about DAC?)



# Biopropane to Infinity & Beyond!

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## Lockheed Martin and Orbex to launch UK into new space age

July 16<sup>th</sup> 2018 – Farnborough International Air Show

*“Their orbital launch vehicle, called Prime, will deliver small satellites into Earth’s orbit, using a single renewable fuel, **bio-propane**, that cuts carbon emissions by 90% compared to hydrocarbon fuels.”*

<https://www.gov.uk/government/news/lockheed-martin-and-orbex-to-launch-uk-into-new-space-age>

*Together in Electric Dreams*

**Thank  
You!**

[Keith.simons@shvenergy.com](mailto:Keith.simons@shvenergy.com)



**CALOR**

BioLPG